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the latter is surprising in that it has been
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given by the authors as a reason for

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Authors, Daizō Kunii, Octave Levenspiel.
Edition, illustrated. Publisher, Wiley,
Original from, the University of Michigan.

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flowing stream of fluid, as shown in Figure R12.3.1. Figure R12.3-1 From Kunii and Levenspiel Fluidization Engineering, Melbourne, FL 32901: Robert E. Krieger Pub. Co. 1969. Reprinted with permission of the publishers

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Adapted from D. Kunii and O. Levenspiel, Fluidization Engineering (Melbourne, Fla.: Robert E. Krieger Publishing Co., 1977). (Note nomenclature change: In the text and lecture, ϵ = porosity, while in this section, ϵ = porosity.) This relationship is a consequence of the fact that the mass of the bed occupied solely

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by the solid particles is the same no matter what the porosity of the bed.

Elements of Chemical Reaction Engineering

Book review Fluidization. Engineering. (Second. D. Kunii and O. Levenspiel, Butterworth-Heinemann, ISBN 0-409-90233-0, f95.00. In revising and

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updating the original text of this book, the scope has been expanded to include fast fluidization as well as bubbling beds, large particle systems such as combustors, the freeboard region and the Geldart classification.

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Kunii, D. and Levenspiel, O. (1991)
Fluidization Engineering. 2nd Edition,
Butterworth-Heinemann, Oxford, 64-69.

Kunii, D. and Levenspiel, O. (1991) Fluidization ...

Fluidization and mass transfer
correlations Minimum fluidization $U_{mf} = \frac{\rho_p g}{\rho_f g} \left(\frac{d_p}{27.2} \right)^2 + 0.0408 Ar$

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– 27.2 velocity [19] Bubble diameter
[20] $D_b = 0.21H^{0.8} (U_0 - U_{mf})^{0.42}$
 $\exp \left[-0.25(U_0 - U_{mf}) \right]$
 $- 0.1(U_0 - U_{mf})$
Bubble velocity [2] $U_b = U_0 - U_e + u_{br}$
 $u_{br} = 0.711 \sqrt{gD_b} \dots$

**Performance of the wide-ranging
models for fluidized bed ...**

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Fluidization Engineering (2nd ed.) by Kunii, D. (ebook)

Fluidization engineering. By Kaizo Kunii and Octave Levenspiel, Butterworth-Heinemann Publisher, 491 pp., 2nd. Ed., \$145 (hard cover), 1991

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The fluidization chamber was a rectangular cuboid with 100, 8, and 40 cm in length, width and height, respectively. The solid feed system was consisted of a bin, a screw conveyor, and an ...

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Engineering, Butterworth, 1991. D.

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Gidaspow, Multiphase flow and fluidization: continuum and kinetic theory description, Elsevier Science & Technology Books, 1993. L.G. Gibilaro, Fluidization-dynamics, Butterworth-Heinemann, 2001.

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MEASUREMENT TECHNIQUES FOR
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(1). They have been applied to physical,
chemical, metallurgical and other
operations, Yang (2). In spite of their

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of Kunii-Levenspiel (3,4) is based on the principles of hydrodynamics and contains three different zones: bubbles, cloud and wake, and emulsion. The main assumptions in this model are that the

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rising bubble follows the Davidson model and also the emulsion phase has the minimum fluidization velocity. The most important

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